# Synergies between biocatalytic methanation of power-to-gas hydrogen and carbon dioxide from alcoholic fermentation

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#### Introduction

Fluctuating energy peaks caused by renewable sources solar and wind require technologies to store energy and to balance fluctuation. A possible storage technology is power-to-gas (P2G), where electric energy is converted to hydrogen by electrolysis. Because of the lack of an adequate hydrogen infrastructure in Germany this P2G-hydrogen can be converted with carbon dioxide into methane.  $CO_2$  can be obtained by breweries, winegrowers or champagne producers with  $CO_2$  excess from alcoholic fermentation.

#### **Biorefinery** cascade

Combination of three technologies, alcoholic fermentation, hydrothermal carbonization (HTC) and biocatalytic methanation, can lead to a  $CO_2$  emission free biorefinery cascade.  $CO_2$  from fermentation and HTC can be used to feed archaea and convert  $CO_2$ into  $CH_4$ . Biomass will be completely converted into fuels and water.

Tab. 1: Production of beer<sup>\*</sup>, wine, sparkling wine/champagne<sup>\*</sup> and bioethanol in Germany (2014) and resulting  $CO_2$  emissions from fermentation (\*data based on sales).

	Production (Germany)	CO <sub>2</sub> production
Beer	$95600000{ m hl}{ m a}^{-1}$	$312000{ m ta^{-1}}$
Wine	$9202000{ m hla^{-1}}$	$69000\mathrm{ta^{-1}}$
Sparkling wine / Champagne	$3174000$ hl a $^{-1}$	$16000{ m ta^{-1}}$
Bioethanol	$726000{ m ta^{-1}}$	$693000{ m ta^{-1}}$
$\sum$		$1090000{ m ta^{-1}}$

Those  $1090000 \text{ ta}^{-1}$  CO<sub>2</sub> can be converted to about  $400000 \text{ ta}^{-1}$  CH<sub>4</sub> which are about **5.6 TW h** of storable energy.

Methanation of carbon dioxide and hydrogen

Following reaction equation shows the conversion of  $CO_2$  and hydrogen to methane.

 $CO_2 + 4H_2 \longrightarrow CH_4 + 2H_2O(I) \qquad \Delta H_R = -165 \text{ kJ mol}^{-1}$ 

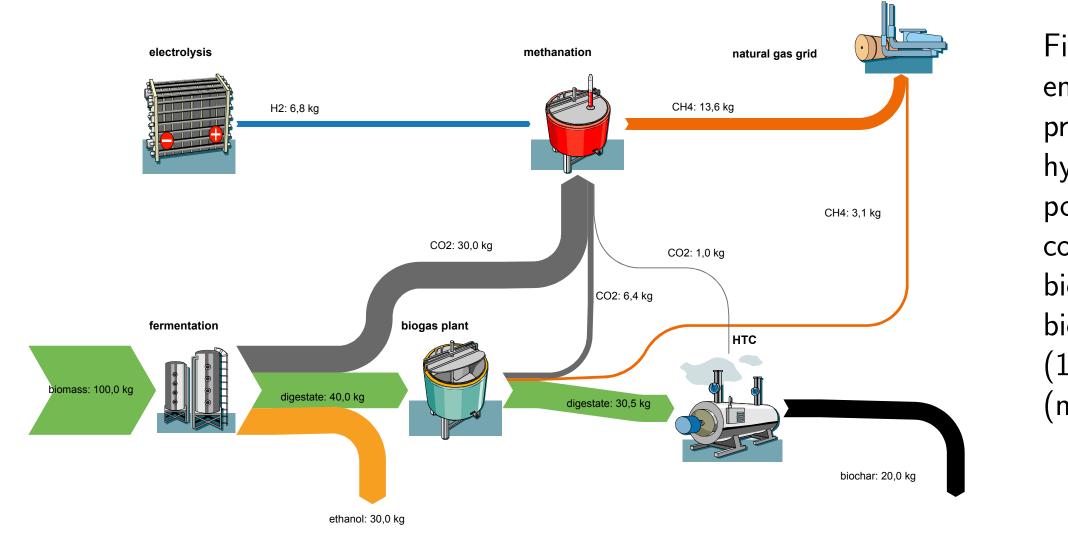


Fig. 2: Scheme of CO<sub>2</sub> emission free biorefinery process. Biomass and hydrogen from power-to-gas are converted to solid (20%)biochar), liquid (30%) bioethanol) and gaseous (16.7%) fuels plus water (not shown).

#### **Experimental Approach**



Except for a chemical methanation (Sabatier process) there are microorganisms (archaea) which metabolize  $CO_2$  to  $CH_4$  under anaerobic conditions. The advantages of this biological over chemical process are moderate process parameters.

Tab. 2: Process parameters of chemical and biological methanation.

Process	Temperature $\vartheta$	Pressure p	needed quality of CO <sub>2</sub> flow
chemical	400 °C	20 bar	high (catalysts)
biological	50 °C to 80 °C	$< 10  { m bar}$	low

#### German energy demand

Netto electricity exports of Germany were 35.5 TW h in 2014. This energy can be used for P2G to balance fluctutating energy production. This energy can be converted via electrolysis into 8.8 bn  $m^3$   $H_2$  and afterwards via methanation into  $2.2 \text{ bn m}^3 \text{ CH}_4$ .

electricity exports = 74.4 TW h

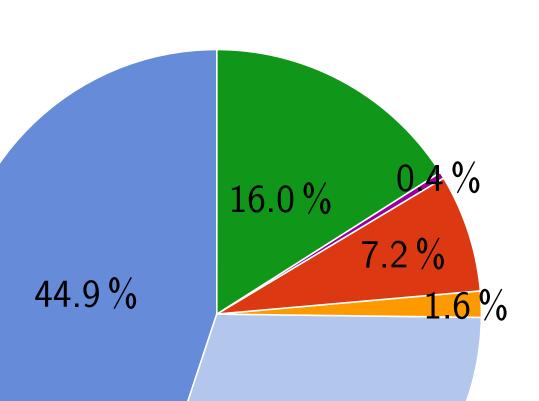




Fig. 3: Left: Methanation in lab scale (0.5 | bottles on hot plate magnetic stirrer) with pressure indication. Middle: Pilot plant scale reactor with magnetic stirrer and baffles. Right: Relative pressure in in lab scale bottles with and without stirring during biological methanation at 65 °C with *Methanothermobacter marburgensis*.

investigation of flexibility - start and stop behaviour

increase conversion rate by investigation of stirring kinetics

pilot scale plant with integrated bioethanol production

feasability for mid-scale brewery in Germany

## Advantages of $CO_2$ form alcoholic fermentation

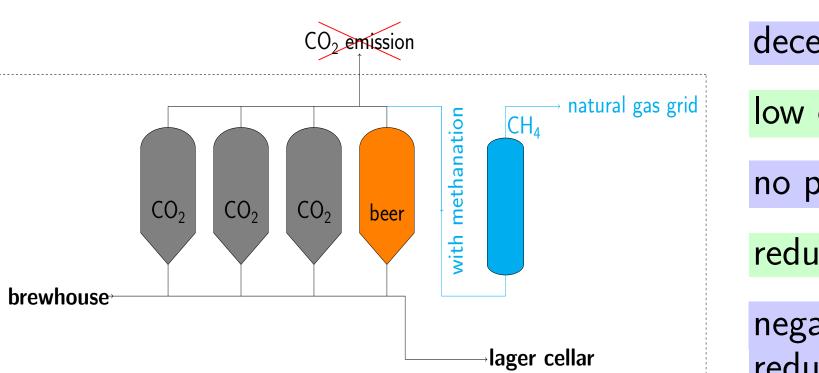


Fig. 4: Schematic fermentation cellar in a brewery

decentral conversion of energy low costs of  $CO_2$  (side stream) no purification needed  $(100\% CO_2)$ reduction of  $CO_2$  emissions of breweries etc. negative CO<sub>2</sub> emissions (GHG emissions reduction potential)

#### electricity imports = 38.9 TW hnetto electricity exports = 35.5 TW h

Fig. 1 shows possible sources for methanation of  $2.2 \text{ bn m}^3 \text{ CO}_2$ . As shown about 1/4 of demanded CO<sub>2</sub> can be provided by alcoholic fermentation. About 30% can be obtained by biogas plants. Missing 44.9% must be obtained by other sources. This figure shows that Fig. 1: Different sources of  $CO_2$  from alcoholic about one half of needed CO<sub>2</sub> is already avail- fermentation and their contribution to convert  $2.2 \text{ bn m}^3 \text{ CO}_2$  to balance fluctuating electricity. able for methanation of 35.5 TW h electric en-Biogas information are based on the known sales in ergy excess. 2013.

29.9% Beer Bioethanol Biogas Wine Sparkling wine/ Other Champagne

with methanation reactor.

infrastructure (piping, vessels) already existent

### References

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